

AMENDMENT

Amendments to the Claims

Please replace all prior versions and listings of claims with the following listing of claims.

LISTING OF CLAIMS:

1. (Currently Amended) A computer based method for determining the cavity size in packed bed systems ~~using correlation or mathematical model, said the~~ method comprising the steps of:

a) ~~obtaining~~ retrieving data parameters related to material properties of the a packed bed system, the parameters including at least: a blast furnace radius (W), an effective bed height (H), a blast velocity (v_b), a tuyere opening (D_t), a void fraction (ϵ), a gas viscosity (μ_g), a particle size (d_p), a shape factor (Φ_s), a density of gas (ρ_g), a density of solid (ρ_s), a coefficient of wall friction (μ_w), an acceleration due to gravity (g), an effective particle diameter given by $d_{eff} = d_p \Phi_s$, an effective bed density given by $\rho_{eff} = \epsilon \rho_g + (1 - \epsilon) \rho_s$, a wall-particle frictional coefficient given by $\mu_w = \tan \Phi_w$, wherein Φ_w is an angle of friction between the wall and the particle, wherein D_r is a cavity diameter, and wherein all units are in SI;

b) ~~calculating~~ determining a the cavity radius (R) for both increasing gas velocity and decreasing gas velocity, ~~using mathematical model the determined cavity radius incorporating the stresses/frictional forces given by as:~~

$$2nR^2 - 2nHR + \frac{pn\beta v_b^2 D_T^2}{2\pi^2 M} \left\{ \ln \frac{W}{2\pi} - \ln \left(R - \frac{D_T}{2\pi} \right) \right\} + \left(\frac{2r_o}{M\pi} (\alpha + \beta v_H) v_H (H - r_o) - \frac{F_{wd}}{M\pi} \right) = 0$$

(29)

and

$$2nR^2 - 2nHR + \frac{pn\beta v_b^2 D_T^2}{2\pi^2 M} \left\{ \ln \frac{W}{2\pi} - \ln \left(R - \frac{D_T}{2\pi} \right) \right\} + \left(\frac{2r_o}{M\pi} (\alpha + \beta v_H) v_H (H - r_o) + \frac{F_{wd}}{M\pi} \right) = 0$$

(28)

respectively; ~~or calculating the cavity radius for both increasing gas velocity and decreasing gas velocity using mathematical equations based on correlation as:~~

$$\frac{D_r}{D_T} = 4.2 \left(\frac{\rho_g v_b^2 D_T}{\rho_{eff} g d_{eff} W} \right)^{0.6} \left(\frac{D_T}{H} \right)^{-0.12} (\mu_w)^{-0.24} \quad (36)$$

$$\frac{D_r}{D_T} = 164 \left(\frac{\rho_g v_b^2 D_T^2}{\rho_{eff} g d_{eff} H W} \right)^{0.80} (\mu_w)^{-0.25} \quad (33)$$

respectively, and

- c) ~~calculating~~ determining a the cavity size using the cavity radius obtained in step (b);
and
d) storing the determined cavity size in a memory.

2. **(Currently Amended)** A method as claimed in claim 1, wherein the data related to material properties of the packed bed comprise at least: bed height, tuyere opening, void fraction, wall-particle friction coefficient, inter-particle frictional coefficient, gas velocity, model width and particle shape factor.

3. **(Cancelled)**

4. **(Original)** A method as claimed in claim 1, wherein the frictional force (F_{wd}) in equations 28 and 29 is given by:

$$F_{wd1} = -\frac{4n\pi\mu_w K h p M}{3\left(1 - \frac{\mu_w K}{n\pi}\right)} \left\{ \left(r_o - \frac{D_T}{2\pi}\right)^3 - \left(R - \frac{D_T}{2\pi}\right)^3 \right\} - 4pn\mu_w K \frac{\beta v_b^2 D_T^2}{4\pi\left(1 + \frac{\mu_w K}{n\pi}\right)} (r_o - R)$$

$$\begin{aligned}
& + \frac{4n\pi\mu_w K \left(\frac{W}{2\pi}\right)^{1-\frac{\mu_w K}{n\pi}} hpM}{\left(1-\frac{\mu_w K}{n\pi}\right)\left(2+\frac{\mu_w K}{n\pi}\right)} \left\{ \left(r_o - \frac{D_T}{2\pi}\right)^{2+\frac{\mu_w K}{n\pi}} - \left(R - \frac{D_T}{2\pi}\right)^{2+\frac{\mu_w K}{n\pi}} \right\} + 4pn\mu_w K \left(\frac{\beta v_b^2 D_T^2}{4\pi}\right) \times \\
& \frac{1}{\left(\frac{W}{2\pi}\right)^{1+\frac{\mu_w K}{n\pi}} \left(1+\frac{\mu_w K}{n\pi}\right)\left(2+\frac{\mu_w K}{n\pi}\right)} \left\{ \left(r_o - \frac{D_T}{2\pi}\right)^{2+\frac{\mu_w K}{n\pi}} - \left(R - \frac{D_T}{2\pi}\right)^{2+\frac{\mu_w K}{n\pi}} \right\} + \frac{2pWn\pi}{\left(2+\frac{\mu_w K}{n\pi}\right)} \left(\frac{W}{2\pi}\right)^{-\frac{\mu_w K}{n\pi}} \times \\
& \left\{ M - \frac{\alpha v_b D_T}{W} - \frac{\beta v_b^2 D_T^2}{W^2} \right\} \left[1 - e^{-C\left(H - \frac{W+D_T}{2\pi}\right)} \right] \left\{ \left(r_o - \frac{D_T}{2\pi}\right)^{2+\frac{\mu_w K}{n\pi}} - \left(R - \frac{D_T}{2\pi}\right)^{2+\frac{\mu_w K}{n\pi}} \right\} + \\
& W \left(\frac{W+D_T}{\pi}\right) \left\{ M - \frac{\alpha_b D_T}{W} - \frac{\beta_b^2 D_T^2}{W^2} \right\} \left[(H - r_o) + \frac{\{e^{-C(H-r_o)} - 1\}}{C} \right]
\end{aligned}$$

5-6. (Cancelled)

7. (Currently Amended) A method as claimed in claim 1, wherein the packed bed systems include system includes at least one of: a blast furnaces furnace, a cupola, a corex, or a catalytic regenerator.

8. (New) A computer based method for determining the cavity size in packed bed systems, the method comprising:

a) retrieving data parameters related to material properties of a packed bed system, the parameters including at least: a blast furnace radius (W), an effective bed height (H), a blast velocity (v_b), a tuyere opening (D_t), a void fraction (ϵ), a gas viscosity (μ_g), a particle size (d_p), a shape factor (Φ_s), a density of gas (ρ_g), a density of solid (ρ_s), a coefficient of wall friction (μ_w), an acceleration due to gravity (g), an effective particle diameter given by $d_{eff} = d_p \Phi_s$, an effective bed density given by $\rho_{eff} = \epsilon \rho_g + (1 - \epsilon) \rho_s$, a wall-particle frictional coefficient given by $\mu_w = \tan \Phi_w$, wherein Φ_w is an angle of friction between the wall and the particle, wherein D_r is a cavity diameter, and wherein all units are in SI;

b) determining a cavity radius (R) for both increasing gas velocity and decreasing gas velocity, the determined cavity radius based on dimensionless numbers given by:

$$\frac{D_r}{D_T} = 4.2 \left(\frac{\rho_g v_b^2 D_T}{\rho_{eff} g d_{eff} W} \right)^{0.6} \left(\frac{D_T}{H} \right)^{-0.12} (\mu_w)^{-0.24} \quad (36)$$

$$\frac{D_r}{D_T} = 164 \left(\frac{\rho_g v_b^2 D_T^2}{\rho_{eff} g d_{eff} H W} \right)^{0.80} (\mu_w)^{-0.25} \quad (33)$$

respectively;

- c) determining a cavity size using the cavity radius obtained in step (b); and
- d) storing the determined cavity size in a memory.

9. **(New)** A method as claimed in claim 8, wherein the data related to material properties of the packed bed comprise at least: bed height, tuyere opening, void fraction, wall-particle friction coefficient, inter-particle frictional coefficient, gas velocity, model width and particle shape factor.

10. **(New)** A method as claimed in claim 8, wherein determining the cavity radius using increasing velocity as given by equation 33 includes using a π -theorem to calculate dimensionless numbers given by:

$$\frac{D_r}{D_T} = 164 \left(\frac{\rho_g v_b^2 D_T^2}{\rho_{eff} g d_{eff} H W} \right)^{0.80} (\mu_w)^{-0.25}.$$

11. **(New)** A method as claimed in claim 8, wherein determining the cavity radius using decreasing velocity as given by equation 36 includes using a π -theorem to calculate dimensionless numbers given by:

$$\frac{D_r}{D_T} = 4.2 \left(\frac{\rho_g v_b^2 D_T}{\rho_{eff} g d_{eff} W} \right)^{0.6} \left(\frac{D_T}{H} \right)^{-0.12} (\mu_w)^{-0.24}.$$

12. (New) A method as claimed in claim 8, wherein the packed bed system includes at least the one of: a blast furnace, a cupola, a corex, or a catalytic regenerator.